Amendments to the Claims

This listing of claims will replace all prior versions and listing of claims in this application.

Listing of claims:

- 1. (Currently Amended) A process for preparing a high impact polystyrene comprising admixing a rubber and styrene monomer in the presence of at least two polymerization initiators and polymerizing the styrene wherein at least one of the at least two polymerization initiators is a grafting initiator and at least one of the at least two polymerization initiators is a non-grafting initiator, and wherein the temperature range for the polymerization is from about 100°C to about 230°C.
- 2. (Original) The process of Claim 1 additionally comprising polymerizing the styrene monomer in the presence of a chain transfer agent.
- 3. (Original) The process of Claim 1 wherein rubber is selected from the group consisting of polybutadiene, styrene-butadiene rubber, styrene-butadiene-styrene rubber, natural rubber, and mixtures thereof.
- 4. (Original) The process of Claim 3 wherein the rubber is polybutadiene.
- 5. (Original) The process of Claim 1 additionally comprising including a solvent in the admixture.
- 6. (Original) The process of Claim 5 wherein the solvent is selected from the group consisting of ethylbenzene, toluene, xylenes, cyclohexane, and mixtures thereof.
- 7. (Original) The process of Claim 5 wherein the solvent is an aliphatic hydrocarbon solvent.
- 8. (Original) The process of Claim 1 wherein the grafting initiator is selected from the group consisting of 1,1-di-(t-butylperoxy)cyclohexane; 1,1-di-(t-bu

amylperoxy)cyclohexane); 1,1-di-(t-butylperoxy)-3,3,5-trimethyl-cyclohexane; OO-t-amyl-O-(2-ethylbexyl monoperoxy-carbonate); OO-t-butyl O-isopropyl monoperoxy-carbonate; OO-t-butyl-O-(2-ethylhexyl)monoperoxy-carbonate; butyl-4,4-di(t-butylperoxy)valerate; Ethyl 3,3-Di-(t-butylperoxy)butyrate; and mixtures thereof.

9. (Original) The process of Claim 8 wherein the grafting initiator is 1,1-di-(t-butylperoxy)cyclohexane.

10.-11. (Cancelled)

- 12. (Original) The process of Claim 1 wherein the high impact polystyrene is prepared using an upflow reactor.
- 13. (Original) The process of Claim 12 wherein the process is a continuous process.
- 14. (Canceled)
- 15. (Currently Amended) The process of Claim <u>1</u>14 wherein the temperatures range for the polymerization is from about 110°C to about 180°C.
- 16. (Original) The process of Claim 1 wherein the grafting initiator is present in an amount of from about 50 to about 1000 parts per million and the non-grafting initiator is present in an amount of from about 100 to about 600 parts per million.
- 17. (Original) The process of Claim 16 wherein the grafting initiator is present in an amount of from about 100 to about 600 parts per million and the non-grafting initiator is present in an amount of from about 100 to about 500 parts per million.

- 18. (Original) The process of Claim 1 wherein the grafting and non-grafting initiators are present in a ratio of grafting to non-grafting initiator of from about 1:10 to about 10:1.
- 19. (Original) The process of Claim 18 wherein the ratio of grafting to non-grafting initiator is from about 1:3 to about 3:1.
- 20. (Original) The process of Claim 19 wherein the weight ratio of styrene to rubber is from about 99:1 to about 7:1.
- 21. (Original) The process of Claim 1 wherein the admixture includes an additive.
- 22. (Original) The process of Claim 21 wherein the additive is selected from the group consisting of chain transfer agents, tale, anti-oxidants, UV stabilizers, lubricants, mineral oil, plasticizers
- 23. (Original) The process of Claim 1 additionally comprising removing residual monomer or solvent from the product high impact polystyrene.
- 24. (Original) A high impact polystyrene prepared by the process of Claim 1.
- 25.-27. (Canceled)